## An efficient method of moments for simulating atmospheric aerosol growth: model description, verification and application

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#### Abstract

The atmospheric aerosol dynamics model (AADM) has been widely used in both comprehensive air quality model systems and chemical transport modeling from road to global scales. The AADM consists of the Smoluchowski coagulation equation (SCE) which describes the atmospheric aerosol size growth due to coagulation. The numerical solution to the SCE undergoing Brownian coagulation in the free molecular regime is a direct challenge because of a stumbling block for the kernel to be expressed by an equivalent linear expression and a predefined lognormal size distribution, which is inconsistent with aerosols having bimodal or multimodal size distribution. Thus, a new mathematical method for solving the SCE without the strong assumption of log-normal size distribution is proposed and developed. This method is verified with a referenced sectional method (SM) with excellent agreement. The accuracy of the method approaches closely to the TEMOM, but overcomes the limitation of the classical log MOM. The computational time of this scheme is largely reduced when comparing to the SM. The new method is successfully implemented to reveal the formation and growth of secondary particles emitted from the vehicle exhaust tailpipe. It is surprisingly found that the formation of new particles only appears in the interface region of the turbulent exhaust jet which is very close to the tailpipe exit, while there is no new particle formation in the strong mixture along the downstream. The new method is finally verified to be an efficient and reliable numerical scheme for studying atmospheric aerosol dynamics.

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12	• Atmospheric aerosol dynamics model
13	• Method of moments
14	Hybridization
15	• Taylor-series expansion method of moments
16	• Method of moments with log-normal size distribution
17	
18	

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- 36 atmospheric aerosol dynamics.

#### **1** Introduction 37

There has been increased recognition of the importance of aerosols to both 38 climate change (Rosenfeld, 2006; Rosenfeld et al., 2014, 2019) and air pollution 39 (Huang et al., 2014; Kumar et al., 2014; Y. Wang et al., 2019; Yao et al., 2018; Yuan 40 et al., 2019). Correspondingly, the inclusion of the aerosol dynamics models in both 41 global chemistry and transport simulations and regional air quality simulations has 42 43 been carried out over half a century (Gama et al., 2019; Hass et al., 2003; Herzog et al., 2004; Jasor et al., 2005; Karydis et al., 2007; Lauer et al., 2005; Sportisse, 2007; 44 Vignati et al., 2004; Whitby & McMurry, 1997; C. Zhou et al., 2016). In all 45 developed aerosol dynamics models, aerosol dynamics which dominates the evolution 46 of particle size distribution are dealt with separately to meet the requirement of 47 numerical simulation. These aerosol dynamic processes usually include nucleation, 48 coagulation, condensation-evaporation, deposition, etc. Brownian coagulation is an 49 important mechanism leading to the instability of aerosols, which is also attracted 50 more interest by scientists than other aerosol dynamics because it is not easily dealt 51 with mathematically. The end result of coagulation is a continuous decrease in 52 particle number concentration and an increase in particle size. The theory for 53 illustrating this phenomenon was originally introduced from Smoluchowski's 54 equation and was then followed by Muller's development (Müller, 1928; Petitti et al., 55 2013). The Muller's equation is expressed as, 56

57 
$$\frac{\partial n(v,t)}{\partial t} =$$

$$\frac{\partial n(v,t)}{\partial t} =$$

 $\frac{1}{2}\int_0^v \beta(v_1, v - v_1)n(v_1, t)n(v - v_1, t)dv_1 - n(v, t)\int_0^\infty \beta(v_1, v)n(v_1, t)dv_1$ 

(1)

59

where particle volume, v, is used rather than particle diameter because the volumes 60 are additive. The first term on the right-hand side of Equation (1) is the rate of 61 formation of particles of size v by smaller particles of sizes  $v_1$  and  $v - v_1$ . The factor 62 1/2 is introduced because collisions are counted twice in the integral. The second 63 term of Equation (1) accounts for the loss of particles of size v by collisions with all 64 other particles. Equation (1) was known as Smoluchowski's Coagulation Equation 65 (SCE), which was further developed later in the community of aerosols to include 66 other aerosol dynamic processes including nucleation, condensation-evaporation, 67 deposition and also to couple with climate models by considering air convection and 68 diffusion. The developed Equation (1) is recognized now as the particle general 69 70 dynamics equation (PGDE), which is the key equation of all weather and air pollution forecast codes, including Weather Research and Forecasting model coupled to 71 Chemistry (WRF-Chem), University of Helsinki Multicomponent Aerosol model and 72 European Air Pollution Dispersion modelling system (EURAD (Ackermann et al., 73 1998; Grabowski et al., 2019; Korhonen et al., 2004; Kukkonen et al., 2012). 74 75 In theory, almost all important aerosol quantities, which determine the

property of aerosol as well as it directly or indirectly affects air pollution and 76

climates, such as number concentration, mass concentration and size distribution of 77 particles, can be obtained by solving the PGDE numerically(Wright et al., 2001). The 78 PGDE is usually solved by numerical methods and there have been some important 79 achievements including the sectional method (SM) (Bruns & Ezekove, 2012; Gelbard 80 et al., 1980; Kostoglou, 2007; Landgrebe & Pratsinis, 1990), method of moments 81 82 (MOM) (Fox et al., 2008; S. Liu, Chan, Lin, et al., 2019; Petitti et al., 2013; Pratsinis, 1988; Rani et al., 2014; Tang & Lin, 2013), Monte Carlo (MC) method (Kraft, 2005; 83 Morgan et al., 2006), and stochastic particle method (Debry et al., 2003; Kruis et al., 84 2012; Menz et al., 2014; Rani et al., 2014; Sabelfeld, 1998). Now, these three 85 different types of numerical methods have been widely applied in weather and air 86 pollution forecast codes. Among all these three numerical methods, the MOM is 87 usually regarded as the most economic one and is also the most suitable to be coupled 88 89 with the air transport equation, such as Navier-Stokes equations (McGraw et al., 2008; Passalacqua et al., 2018; Yu & Lin, 2018) To be noted here, the MOM with 90 predefined log-normal size distribution is still the classical method used in the most 91 common weather and air pollution forecast codes, such as WRF-Chem and EURAD 92 (Cai et al., 2016; Gama et al., 2019). It should be noted that the SM is also used for 93 94 modeling aerosol dynamics in nuclear reactor safety (Herranz et al., 2018).

95 The key of the MOM is to implement a transformation from particle size 96 distribution (PSD) function space,  $\{n(v)\}$  in Equation (1), to the space of moments,  $\{m_k\}$ . When transferring from  $\{n(v)\}$  to  $\{m_k\}$ , the closure problem for ordinary 97 differential equations (ODEs) appears which needs to be resolved using closure 98 schemes. There have been several schemes to achieve closure, which can be divided 99 into two categories, namely quadrature-based MOM (QBMOM) and non-quadrature-100 based MOM (NBMOM). The predefined particle size distributed method, pth-order-101 polynomial MOM, MOM with interpolative closure (MOMIC) and Taylor series 102 expansion MOM belong to the NBMOM. An advantage of the NBMOM is that the 103 104 transferred moment ODEs can be written as its explicit form (Yu & Lin, 2018). It should be noted that the QBMOM, especially Gaussian quadrature MOM (QMOM 105 and direct QMOM (DQMOM)) (Marchisio & Fox, 2005; Robert McGraw, 1997a) is 106 107 the most widely used MOM to couple with computational fluid dynamics (CFD) until 108 nowadays. Among all the NBMOMs, the predefined log-normal MOM was the first 109 proposed for solving PGDE (Cohen & Vaughan, 1971), and now it governs the establishment of atmospheric aerosol models, including WRF-Chem and EURAD. 110 When implementing the log-normal MOM by transferring from the particle size 111 distribution function space,  $\{n(v)\}$  to the space of moments,  $\{m_k\}$ , the collision 112 kernel must be written as an equivalent linear expression for  $v^p v_1^q$  (p and q are 113 arbitrary real numbers). This requirement limits the application of log MOM because 114 some kernels cannot easily be obtained with an equivalent linear expression for  $v^p v_1^q$ . 115 Although the QBMOM is the widely used MOMs today due to main contributions 116 from the research groups of Fox (Heylmun et al., 2019; Kong & Fox, 2017; 117 Marchisio & Fox, 2005; Vikas et al., 2013) and McGraw (McGraw et al., 2008; 118 McGraw, 1997b), the NBMOM, such as the log MOM and TEMOM, can still find its 119

- 120 wide applications due to their high numerical efficiency without eigensystems'
- 121 calculation and ill-conditioned matric problems.
- 122

Brownian coagulation in the free molecular is a key mechanism affecting the

- evolution of aerosol size distribution with particle Knudsen number (Kn =  $\frac{\lambda}{r}$ , where  $\lambda$
- is the mean free path of air, and r is particle diameter) larger than 50 (Park et al.,
- 1999a). The collision kernel in this regime has a term  $(1/v + 1/v_1)^{1/2}$ , which is the 125 major stumbling block for the kernel to be expressed by an equivalent linear 126 expression, so does the transfer of SCE to the moment ODEs. Some efforts have been 127 made to overcome this technical difficulty. The most success is the strategy proposed 128 by Lee et al. (1984), in which the factor  $(1/v + 1/v_1)^{1/2}$  was substituted by  $b[(1/v_1)^{1/2}]$ 129 v)<sup>1/2</sup> + (1/ $v_1$ )<sup>1/2</sup>]; the SCE can then be transferred to moment ODEs with both 130 implicit and explicit moments. In order to achieve the final closure of moment ODEs, 131 Equation (11) below is needed. Unfortunately, the value of b is an unmanageable 132 issue in Equation (9) below, which has to be obtained through solving integral 133 equations with varying initial particle size distributions. Pratsinis (1988) then further 134 developed and expressed the term, b, as a function of geometric standard deviation of 135 particle size distribution. However, both of their studies have the limitation that the 136 expression of the value b has to be determined numerically in advance, which 137 138 inevitably leads to uncertain in mathematics. Hence, a high efficient and precise method becomes essential to approximate this collision kernel. 139
- 140 The TEMOM was proposed by Yu et al. (2008) to solve SCE. The key of the 141 TEMOM is to approximate any expressions using their truncated Taylor expansion series with adjusted errors, thus the technical difficulty in the log MOM might be 142 overcome by the TEMOM. Although the TEMOM has been successfully applied to 143 solve the SCE due to Brownian coagulation in the free molecular regime, (1/v +144  $1/v_1$ <sup>1/2</sup> and implicit moments are both implemented by the Taylor-series expansion 145 technique. Whether  $(1/v + 1/v_1)^{1/2}$  is implemented by the TEMOM and implicit 146 moments are implemented by the log MOM simultaneously or conversely, it remains 147 an open question. 148

149 In the present study, a new method to explicitly solve the SCE undergoing Brownian coagulation in the free molecular regime is presented. The underlying idea 150 of this method is that the approximations of collision kernel and explicit moments are 151 achieved by the hybridization of the well-established log MOM and TEMOM. For 152 distinguishing this new hybrid method from other MOMs, a hybrid TEMOM-log 153 MOM is used. Since there are two different hybrid processes involvement, namely 154 hybrid TEMOM-log MOM (I) and hybrid TEMOM-log MOM (II), are used for their 155 distinguishment. The SM as a reference is used to validate this new scheme of hybrid 156 TEMOM-log MOM, which has regarded as an exact solution of SCE by the aerosol 157 society (Otto et al., 1999) as well as our previous works (Yu et al., 2016; Yu & Lin, 158 2017a). In addition, the results from both TEMOM and log MOM are presented for 159 comparative studies. The moment ODEs obtained from the proposed scheme have the 160 explicit expressions, thus to be easier programed than the well-established log MOM. 161

162 The newly proposed hybrid TEMOM-log MOM (I) is further utilized to study the 163 formation and growth of secondary particles emitted from the vehicle exhaust tailpipe, 164 in which an advanced parameterized model for binary homogeneous nucleation of 165 sulfuric acid-water vapors is introduced. The competing processes of binary 166 nucleation, condensation and coagulation are clearly revealed.

The paper is organized as follows: In Section 2, the model description related 167 to the hybrid TEMOM-log MOM method is presented, and the numerical errors are 168 fully analyzed. In Section 3, the numerical details of studied cases are provided and 169 all the governing equations are dealt with a normalized method. In Section 4, the 170 results and discussion are presented for the comparison among new hybrid TEMOM-171 log MOM, TEMOM, log MOM, and SM, and the validation of the new method is 172 carried out. In this section, the new scheme is further utilized to study the exhaust 173 particles emitted from the vehicle tailpipe. The factors affecting the secondary 174 175 nanoparticle formation and subsequent growth in a turbulent jet exhaust plume are revealed. 176

#### 177 2 Materials and Methods

In the present study, Brownian coagulation in the free molecular regime is
considered because it is the most difficult to deal with using the MOM
(Pratsinis,1988). For the studied case, the coagulation kernel is given by (Friedlander,
2000):

182 
$$\beta(v, v_1) = B_1 (1/v + 1/v_1)^{1/2} (v^{1/3} + v_1^{1/3})^2 \qquad (2)$$

183 where  $B_1 = (3 / 4\pi)^{1/6} (6k_BT / \rho_p)^{1/2}$ ,  $k_B$  is the Boltzmann constant, T is the gas

184 temperature and  $\rho_p$  is the mass density of the particles.

In order to implement the MOM, the system of Equation (1) is transferred to a system of moment ODEs with respect to the moment. The moment transformation involves multiplying Equation (1) by v and then integrating over the entire particle size distribution, and then the moment transformed equations of the PSD are obtained (Lee et al., 1984):

190 
$$\frac{\mathrm{d}m_k}{\mathrm{d}t} = \frac{1}{2} \int_0^\infty \int_0^\infty \kappa(v, v_1, k) n(v, t) n(v_1, t) \mathrm{d}v \mathrm{d}v_1 \qquad (3)$$

191 where  $\kappa(v, v_1, k) = [(v + v_1)^k - v^k - v_1^k]\beta(v, v_1)$  and the moment  $m_k$  is defined 192 by:

193 
$$m_k = \int_0^\infty v^k n(v) \,\mathrm{d}v \tag{4}$$

194 The dynamic behavior of an aerosol can be described from the rate of change of its

195 first three moments(Pratsinis, 1988). According to the present study on the log MOM

and TEMOM, only the first three moments are considered here,

$$\kappa(v, v_1, k) = [(v + v_1)^k - v^k - v_1^k]\beta(v, v_1)$$
$$= \begin{cases} -\beta(v, v_1), & k = 0, \\ 0, & k = 1, \\ 2vv_1\beta(v, v_1), & k = 2. \end{cases}$$
(5)

198 2.1. Two technical difficulties in the MOM

197

199 If only k = 0, 1 and 2 are involved, Equation (3) can be written as

$$\begin{cases} \frac{\mathrm{d}m_{0}}{\mathrm{d}t} = -\frac{1}{2} \int_{0}^{\infty} \int_{0}^{\infty} \beta(v, v_{1}) n(v, t) n(v_{1}, t) \mathrm{d}v \mathrm{d}v_{1}, \\ \frac{\mathrm{d}m_{1}}{\mathrm{d}t} = 0, \\ \frac{\mathrm{d}m_{2}}{\mathrm{d}t} = \int_{0}^{\infty} \int_{0}^{\infty} v v_{1} \beta(v, v_{1}) n(v, t) n(v_{1}, t) \mathrm{d}v \mathrm{d}v_{1}. \end{cases}$$
(6)

200 The purpose of the MOM is to remove an integral operator on the right hands of

201 Equation (6). Unfortunately, two essential technical difficulties arise from the particle

size distribution function space,  $\{n(v)\}$ , to the space of moments,  $\{m_k\}$ , i.e. the

203 binary polynomial approximation and the closure function for any order moment.

204 2.1.1 Binary polynomial approximation

To introduce the Equation (4) into Equation (6), the collision kernel,  $\beta(v, v_1)$ must be expressed as a binary additive form, i.e.,

$$\tilde{\beta}(v,v_1) = \sum_{p \in R} \sum_{q \in R} a_{pq} v^p v_1^q \approx \beta(v,v_1) \quad (7)$$

where *p* and *q* are arbitrary real numbers,  $a_{pq}$  is coefficient. Unfortunately, the presence of the term  $(1/v + 1/v_1)^{1/2}$  in Equation (2) makes the binary additive form unavailable.

210 2.1.2 Closure function

Even if Equation (7) is available and the terms on the right sides of Equation (6)

- can be expressed as functions of moments, these moments are usually not explicit
- 213 which makes the non-closure of transferred moment ODEs. A general closure
- 214 function that can be used to replace any k-th moments becomes necessary. In

Equation (6), only the first three moments, namely  $m_0$ ,  $m_1$  and  $m_2$ , are explicit, and thus the general closure function can be expressed as,

 $m_k = f_{\text{closure}}(m_0, m_1, m_2) \quad (8)$ 

217 where k is an arbitrary real number.

It should be noted that both log MOM and TEMOM have the same above mentioned problems, and the corresponding solutions of them have been given by

direct and explicit formulations as Equations (7) and (8).

221 2.2. Two polynomial approximations to the kernel in the free-molecule regime

In the previous work of Lee et al (1984), the term  $(1/v + 1/v_1)^{1/2}$  is approximated as

225 
$$\left(\frac{1}{\nu} + \frac{1}{\nu_1}\right)^{1/2} \approx b\left(\frac{1}{\nu^{1/2}} + \frac{1}{\nu_1^{1/2}}\right)$$
 (9)

226 where

$$b = \int_0^\infty \int_0^\infty v^k \beta(v, v_1) n(v, t) n(v_1, t) dv dv_1$$
$$\times \left\{ \int_0^\infty \int_0^\infty \left[ \frac{\left( \frac{1}{v^{1/2}} + \frac{1}{v_1^{1/2}} \right)}{(v + v_1)^{1/2}} \right] \times v^k \beta(v, v_1) n(v, t) n(v_1, t) dv dv_1 \right\}^{-1}$$

227

(10)

To obtain the coefficient b in Equation (10), the numerical calculation must be 228 carried out. In addition, b is a value depending on the initial geometric standard 229 deviation,  $\sigma_0$  in the work of Lee et al. (1984) and Pratsinis (1988). It implies that b 230 has different values for different particle size distribution. This makes the approach to 231 deal with the uncertainty of  $(1/v + 1/v_1)^{1/2}$  in mathematics. Although Pratsinis 232 (1988) tried to write b as a function of  $\sigma_0$ , the relative errors to real values of such an 233 approach cannot be obtained. Furthermore, for calculating the value of b, many 234 hypotheses and simplifications have to be involved, including the assumption of 235 time-dependent log-normal size distribution. It leads to the motivation for developing 236 a more reliable way in order to deal with the approximation of  $(1/v + 1/v_1)^{1/2}$  in 237 238 the present study.

The collision kernel in the free molecular regime, i.e. Equation (2), can be further expressed if the log MOM is implemented as follows,

$$\beta(v, v_1) = Kb_k (v_1^2 v_1^{-\frac{1}{2}} + 2v_1^{\frac{1}{3}} v_1^{-\frac{1}{6}} + v_1^{\frac{1}{6}} + v_1^{\frac{1}{6}} + 2v_1^{-\frac{1}{6}} v_1^{\frac{1}{3}} + v_1^{-\frac{1}{2}} v_1^{\frac{2}{3}})$$

$$\triangleq \tilde{\beta}_{\text{Log}}(v, v_1) \qquad (11)$$

Here, the approximating kernel  $\tilde{\beta}_{Log}(v, v_1)$  is called a log-normal kernel (Log-kernel).

243 2.2.2. Binary Taylor expansion kernel (Taylor-kernel)

In the TEMOM, the term  $(1/v + 1/v_1)^{1/2}$  is approximated with a binary

additive form by implementing a binary Taylor-series expansion technique

(Mingzhou Yu et al., 2008). Without loss of generality,  $f(v, v_1) = (v + v_1)^{1/2}$  can then be defined as,

 $f(v, v_1) =$ 

248 
$$f(u,u) + \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right] f(u,u) +$$

249 
$$\frac{1}{2!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^2 f(u,u) + \dots +$$

$$250 \quad \frac{1}{n!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^n f(u,u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v-u)\frac{\partial}{\partial v} \right]^{n+1} f(u+u) + \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v}$$

251 
$$\theta(v-u), u+\theta(v_1-u)), (0 < \theta < 1)$$
. (12)

252 The error  $R_n$  is denoted as

255

253 
$$R_n = \frac{1}{(n+1)!} \left[ (v-u)\frac{\partial}{\partial v} + (v_1 - u)\frac{\partial}{\partial v_1} \right]^{n+1} f(u+\theta(v-u), u+\theta(v_1 - u)), \quad (13)$$

and the absolute error  $|R_n|$  is denoted as

$$|R_n| \le \frac{M}{(n+1)!} (|v-u| + |v_1-u|)^{n+1} = \frac{M}{(n+1)!} \rho^{n+1} (|\cos \alpha| + |\sin \beta|)^{n+1}$$
$$= \frac{(\sqrt{2})^{n+1}}{(n+1)!} M \rho^{n+1} \qquad (14)$$

where *M* is a positive number and  $\rho = \sqrt{(v-u)^2 + (v_1 - u)^2}$ . When  $\rho \to 0$ , i.e.,

257  $v \to u$  and  $v_1 \to u$  simultaneously, the absolute error  $|R_n| \to 0$  and the rate of

convergence is  $O(\rho^{n+1})$ . It implies the binary additive form in Equation (12) is

theoretically reasonable when the volume of aerosol particles approaches the average

value. If the Taylor-series expansion point is u, the term  $(1/v + 1/v_1)^{1/2}$  is

approximated by the following expression,

 $\beta(v,v_1)$ 

$$(v+v_1)^{1/2} \approx \frac{3\sqrt{2u}}{8} + \frac{3\sqrt{2}v}{8\sqrt{u}} + \frac{3\sqrt{2}v_1}{8\sqrt{u}} - \frac{\sqrt{2}v^2}{32u^{3/2}} - \frac{\sqrt{2}vv_1}{16u^{3/2}} - \frac{\sqrt{2}v_1^2}{32u^{3/2}}.$$
 (15)

262 Then the collision kernel in the free-molecule regime is now approximated as follows:

$$\approx B_1 \left[ \frac{3}{8} (2u)^{\frac{1}{2}} (2v^{\frac{1}{6}}v_1^{-\frac{1}{2}} + 2v^{-\frac{1}{6}}v_1^{-\frac{1}{6}}) + \frac{3}{8} (\frac{2}{u})^{\frac{1}{2}} (2v^{\frac{7}{6}}v_1^{-\frac{1}{2}} + 4v^{\frac{5}{6}}v_1^{-\frac{1}{6}} + 2v^{\frac{1}{2}}v_1^{\frac{1}{6}}) \right]$$
$$- \frac{1}{32} (\frac{2}{u^3})^{\frac{1}{2}} (4v^{\frac{5}{6}}v_1^{\frac{5}{6}} + 4v^{\frac{7}{6}}v_1^{\frac{1}{2}} + 2v^{\frac{3}{2}}v_1^{\frac{1}{6}} + 2v^{\frac{13}{6}}v_1^{-\frac{1}{2}} + 4v^{\frac{11}{6}}v_1^{-\frac{1}{6}}) \right]$$
$$\triangleq \tilde{\beta}_{\text{Taylor}}(v, v_1); \quad (16)$$

Here, the approximating kernel  $\tilde{\beta}_{Taylor}(v, v_1)$  is called binary Taylor expansion kernel (Taylor-kernel).

Substituting the log-kernel into Equation (11) and the Taylor-kernel in Equation
(16) into the moment ODEs of Equation (5) results in the following system,
respectively,

$$\begin{cases} \frac{\mathrm{d}m_0}{\mathrm{d}t} = -\frac{1}{2} \int_0^\infty \int_0^\infty \tilde{\beta}_{\mathrm{Log}}(v, v_1) n(v, t) n(v_1, t) \mathrm{d}v \mathrm{d}v_1 \\ \frac{\mathrm{d}m_1}{\mathrm{d}t} = 0 \\ \frac{\mathrm{d}m_2}{\mathrm{d}t} = \int_0^\infty \int_0^\infty v v_1 \tilde{\beta}_{\mathrm{Log}}(v, v_1) n(v, t) n(v_1, t) \mathrm{d}v \mathrm{d}v_1. \end{cases}$$
(17)

269 and

263

$$\begin{cases} \frac{\mathrm{d}m_0}{\mathrm{d}t} = -\frac{1}{2} \int_0^\infty \int_0^\infty \tilde{\beta}_{\mathrm{Taylor}}(v, v_1) n(v, t) n(v_1, t) \mathrm{d}v \mathrm{d}v_1 \\ \frac{\mathrm{d}m_1}{\mathrm{d}t} = 0 \\ \frac{\mathrm{d}m_2}{\mathrm{d}t} = \int_0^\infty \int_0^\infty v v_1 \tilde{\beta}_{\mathrm{Taylor}}(v, v_1) n(v, t) n(v_1, t) \mathrm{d}v \mathrm{d}v_1. \end{cases}$$
(18)

#### 270 2.3. Two closure functions in the MOM

Both log MOM and TEMOM have been widely verified to be promising 271 methods for solving SCE with very little computational costs. As discussed in Section 272 2.1, both Equations. (17) and (18) are needed to be further closed using suitable 273 closure functions. In the log MOM, the closure function is obtained based on an 274 assumption of time-dependent log-normal size distribution, whereas in the TEMOM 275 the closure function is obtained by expanding  $v^k$  within a manageable error. If the log 276 MOM closure function (Lee et al., 1984) is applied to Equation (17) and the TEMOM 277 closure function (Yu et al., 2008) is applied to Equation (18), the new schemes are 278 279 presented as below.

#### 280 2.3.1. Hybrid TEMOM-log MOM (I)

281 In the TEMOM, the closure function has the following expression,

$$m_{k} = \left(\frac{u^{k-2}k^{2}}{2} - \frac{u^{k-2}k}{2}\right)m_{2} + \left(-u^{k-1}k^{2} + 2u^{k-1}k\right)m_{1} + \left(u^{k} + \frac{u^{k}k^{2}}{2} - \frac{3u^{k}k}{2}\right)m_{0}$$
  
$$\triangleq m_{k_{\text{Taylor}}}, \ \left(u = \frac{m_{1}}{m_{0}}\right) \quad (19)$$

As Equation (19) is applied to Equation (17), a new scheme of hybrid TEMOM-log
MOM (I) is derived,

$$\begin{cases} \frac{dm_0}{dt} = B_1 b \frac{m_0^{11/6} (41m_0^2 m_2^2 - 190m_0 m_1^2 m_2 - 2443m_1^4)}{648m_1^{23/6}} \\ \frac{dm_1}{dt} = 0 \\ \frac{dm_2}{dt} = -B_1 b \frac{65m_0^2 m_2^2 - 670m_0 m_1^2 m_2 - 1987m_1^4}{324m_0^1 m_2^6}. \end{cases}$$
(20)

285 2.3.2. Hybrid TEMOM-log MOM (II)

In the log MOM, the closure function is obtained by assuming the log-normal particle size distribution (Lee et al., 1984),

288 
$$m_k = m_0^{1 - \frac{3}{2}k + \frac{1}{2}k^2} m_1^{2k - k^2} m_2^{-\frac{1}{2}k + \frac{1}{2}k^2}.$$
 (21)

The derivation of Equation (21) is shown in Appendix 7.3. As Equation (21) is

- applied to Equation (18), another new scheme of hybrid TEMOM-log MOM (II) for
- 291 solving SCE can be expressed as

284

$$\begin{cases} \frac{dm_0}{dt} = -\frac{B_1}{2} \frac{\sqrt{2}m_0^{\frac{59}{36}}}{16m_1^9 m_2^{\frac{29}{36}}} \begin{pmatrix} -\frac{11}{6}m_1^{\frac{1}{9}}\frac{11}{m_2^6} + 12m_0^{\frac{2}{3}}m_1^{\frac{2}{2}}\frac{22}{9}m_2^{\frac{2}{3}} + 11m_0^{\frac{2}{9}}m_1^{\frac{2}{9}}\frac{1}{m_2^2} + 12m_0^{\frac{7}{18}}m_1^{\frac{7}{18}}m_2^{\frac{7}{18}} \\ + 24m_0^{\frac{2}{9}}m_1^{\frac{2}{9}}\frac{2}{m_2^9} - \frac{1}{2}m_0^{\frac{31}{9}}m_1^{\frac{1}{9}}\frac{1}{m_2^9} - 2m_0^{\frac{19}{18}}m_1^{\frac{5}{9}}m_2^{\frac{19}{2}} - 2m_0^{\frac{19}{18}}m_1^{\frac{5}{18}}m_1^{\frac{19}{18}}\frac{1}{m_1^{\frac{1}{18}}} + 12m_1^{\frac{34}{9}} \end{pmatrix} \\ \frac{dm_1}{dt} = 0 \\ \frac{dm_2}{dt} = -\frac{B_1}{2}\frac{\sqrt{2}m_0^{\frac{25}{36}}}{\frac{41}{9}m_2^{\frac{5}{36}}} \begin{pmatrix} \frac{23}{6}m_1^{\frac{1}{9}}m_2^{\frac{31}{9}} - 24m_0^{\frac{11}{9}}m_1^{\frac{16}{3}}m_2^{\frac{5}{9}} - 12m_0^{\frac{5}{3}}m_1^{\frac{49}{9}}m_2^{\frac{23}{18}} + 2m_0^{\frac{31}{9}}m_1^{\frac{19}{9}}m_2^{\frac{16}{9}} + 2m_0^{\frac{55}{18}}m_1^{\frac{5}{3}}m_2^{\frac{8}{9}} \\ \frac{37}{2}m_1^{\frac{11}{18}}m_2^{\frac{5}{9}} - 24m_0^{\frac{19}{9}}m_1^{\frac{19}{18}}m_2^{\frac{5}{9}} - 12m_0^{\frac{5}{9}}m_1^{\frac{19}{9}}m_2^{\frac{23}{18}} + 2m_0^{\frac{5}{9}}m_1^{\frac{31}{9}}m_2^{\frac{9}{9}} + 2m_0^{\frac{55}{18}}m_1^{\frac{5}{3}}m_2^{\frac{8}{9}} \\ + 2m_0^{\frac{37}{18}}m_1^{\frac{13}{18}}m_2^{\frac{5}{9}} + m_0^{\frac{5}{9}}m_1^{\frac{9}{9}}m_2^{\frac{9}{9}} - 12m_0^{\frac{5}{9}}m_1^{\frac{19}{9}}m_2^{\frac{23}{18}} + 2m_0^{\frac{13}{6}}m_1^{\frac{19}{9}}m_2^{\frac{5}{9}} + 2m_0^{\frac{55}{18}}m_1^{\frac{5}{18}}m_2^{\frac{8}{9}} \\ + 2m_0^{\frac{37}{18}}m_1^{\frac{13}{18}}m_2^{\frac{5}{9}} + m_0^{\frac{5}{9}}m_1^{\frac{9}{9}}m_2^{\frac{9}{9}} - 12m_0^{\frac{19}{9}}m_1^{\frac{19}{9}}m_2^{\frac{13}{18}} - 12m_0^{\frac{59}{18}}m_1^{\frac{11}{9}}m_2^{\frac{5}{9}} - 12m_0^{\frac{59}{9}}m_1^{\frac{19}{9}}m_2^{\frac{19}{9}} - 12m_0^{\frac{59}{9}}m_1^{\frac{19}{9}}m_2^{\frac{13}{18}} - 12m_0^{\frac{59}{18}}m_1^{\frac{19}{9}}m_2^{\frac{19}{9}} \\ + 2m_0^{\frac{19}{18}}m_1^{\frac{19}{18}}m_2^{\frac{5}{9}} + m_0^{\frac{19}{9}}m_1^{\frac{9}{9}}m_2^{\frac{9}{9}} - 12m_0^{\frac{19}{9}}m_1^{\frac{19}{9}}m_2^{\frac{19}{18}} - 12m_0^{\frac{19}{9}}m_1^{\frac{19}{9}}m_2^{\frac{19}{18}} - 12m_0^{\frac{19}{9}}m_1^{\frac{19}{9}}m_2^{\frac{19}{18}} - 12m_0^{\frac{19}{9}}m_1^{\frac{19}{18}} - 12m_0^{\frac{19}{18}}m_1^{\frac{19}{18}} \\ + 2m_0^{\frac{19}{18}}m_1^{\frac{19}{18}}m_2^{\frac{19}{18}} + m_0^{\frac{19}{18}}m_1^{\frac{19}{18}}m_2^{\frac{19}{18}} - 12m_0^{\frac{19}{18}}m_1^{\frac{19}{18}} - 12m_0^{\frac{19}{18}}m_1^{\frac{19}{1$$

292

#### 293 2.4. Family of TEMOM-log MOM

According to the above-mentioned schemes, four MOM models can be classified for solving SCE through adjusting the combination of the binary polynomial kernels and the closure functions, which constitutes a family of TEMOM-log MOM



297



#### Figure 1 Spanning map of the family of TEMOM-log MOM.

299

Both the log MOM and TEMOM have been verified as reliable methods for solving SCE. However, the newly proposed and developed hybrid TEMOM-log MOM (I) and (II) have never been verified before. Equations (20) and (22) have explicit expressions, thus the numerical algorithms can be written using a very simple way. In the well-established log MOM widely used in AADM (Pratsinis, 1988), however, the ODEs have to be closed using a log-normal size distributed assumption.

#### **306 3 Computational description**

The SM is selected as a reference and is implemented under the same condition as the hybrid TEMOM-log MOM (I) and (II) models. The relative errors of the hybrid TEMOM-log MOM (I) and (II) models to the SM are discussed in Section 4. In the
present study, the SM model is usually used for validating MOMs which is solved
using the same computer code as that used in (Yu & Lin, 2017b). The log MOM and
TEMOM are also implemented for comparison purposes. The solution with the
assumption of an initial log-normal particle size distribution is used (Barrett & Jheeta,

1996). Hence, *k*-th moment can be represented by

$$m_k = M_k \left( N_0 v_{g_0}^k \right) (23)$$

315 where  $v_{g_0}$  is the initial geometric mean volume. When the normalized terms are

implemented in the moment ODEs as shown in Equations (20) and (23),  $N_0$  and  $v_{g_0}$ 

317 are included in the normalized time. Under this condition, the dimensionless time with

318 respect to the coagulation kernel in the free molecular regime is

$$\tau = B_1 N_0 v_{g_0}^{1/6} t \tag{24}$$

319 When the Equation (25) is introduced into Equations (20) and (22), the

normalized equations for the hybrid models (I) and (II) are obtained, which are

321 presented in Appendix 7.4. The initial moments can be expressed as

 $M_{k0} = \chi^{k^2} \tag{25}$ 

where  $\chi = e^{(3\ln\sigma_{g_0})^2/2}$ . The normalization using Equations (23-25) are applied to the study in Sections 4.1 and 4.3. To be consistent with the study in Yu et al. (2009).,  $N_0 = 5.0 \times 10^{19} \, \text{#/m}^3$  and  $d_{g_0} = 0.4 \times 10^{-9} \, \text{m} \cdot d_{g_0}$  is selected for the diameter of

325 the  $H_2SO_4$  molecular.

#### 326 4 Results and Discussion

Both the numerical precision and efficiency of the newly proposed method for solving SCE are evaluated to verify its reliability in Sections 4.1 and 4.2. In Section 4.3, the application of the newly proposed method in the study of the formation and growth of secondary particles in the turbulent exhaust jet plume is discussed.

331 4.1 Model validation

The purpose is to verify the numerical precision of the newly proposed and developed hybrid (I) and (II) models. To achieve this, the hybrid models (I) and (II),

- log MOM, TEMOM and SM are applied to solve the same SCE under the same
- conditions. Four crucial moments, namely  $M_0$ ,  $M_{1/3}$ ,  $M_{2/3}$ , and  $M_{27}$  are evaluated.
- 336 The relative errors of the k-th moments of the investigated methods of moments to the
- 337 SM are expressed as:

$$\operatorname{RE}(\%) = \frac{M_k(\operatorname{MOM}) - M_k(\operatorname{SM})}{M_k(\operatorname{SM})}$$
(26)

- 338 where  $M_k$  (MOM) is the *k*-th moments obtained from the investigated method of
- moments and  $M_k$  (SM) is the corresponding moments obtained from the referenced
- 340 SM. All numerical calculations are implemented using the fourth-order Runge–Kutta
- 341 method with a fixed time step of 0.001. The SM, log MOM and TEMOM are verified
- 342 in Park et al. (1999b), Yu et al. (2008; 2015) and Yu & Lin (2017b).



Fig. 2. The variance of *k*-th moments with time produced by the family of TEMOM-log MOM

- Fig.2 shows the comparison of the variances of four essential moments with
- respect to time among these two new hybrid models, log MOM (Lee et al., 1984), and
- 348 TEMOM (Yu et al., 2008). In the numerical calculation, the initial geometric standard
- deviation of particle number distribution,  $\sigma_{g0} = 1.2$ . The zeroth moment,  $M_0$ ,
- represents the particle number concentration; the 1/3th moment,  $M_{1/3}$ , is a quantity
- 351 characterizing particle surface concentration. The 2/3th moment  $(M_{2/3})$  and 2th
- moment  $(M_2)$  have no actual physical meanings, but these two moment variables are
- 353 essential parts to get other important physical quantities of aerosols such as geometric
- standard deviation of particle number distribution is given in Equation (27). For three
- investigated moments, namely  $M_0$ ,  $M_{1/3}$ , and  $M_{2/3}$ , all curves overlap with each
- other, while for  $M_2$  only the hybrid TEMOM-log MOM (II) deviates slightly from the
- 357 other three models. The comparison implies that the hybrid TEMOM-log MOM (I),
- log MOM and TEMOM have nearly the same numerical precision for solving SCE
- undergoing Brownian coagulation in the free molecular regime. The hybrid TEMOM-
- 360 log MOM (II) has only a slight difference with the other three models.

361



Fig. 3. Relative errors of *k*-th moments of the family of TEMOM-log MOM to the referenced SM in the free molecular regime

For a better evaluation of the reliable new method, the relative errors (REs) of the 367 four moments of the family of TEMOM-log MOM are investigated to the referenced 368 SM as shown in Fig. 3. The SM is usually considered as an exact numerical solution 369 to the SCE (Otto et al., 1999). It is clear that these four methods in the family of 370 TEMOM-log MOM have almost the same variance trend and the maximum relative 371 error of the hybrid TEMOM-log MOM (II) has found in  $M_0$ ,  $M_{1/3}$ ,  $M_{2/3}$ , and  $M_2$ , 372 respectively. In addition, the other three methods almost overlap with each other 373 especially for  $M_{2/3}$ . The relative errors of these four methods almost overlap with 374 each other again as  $\tau \to 10^2$  for  $M_0$ ,  $M_{2/3}$ , and  $M_2$ , respectively. It is concluded that 375 the newly proposed and developed hybrid models, especially the TEMOM-log MOM 376 (I) has nearly the same numerical accuracy as the TEMOM and log MOM. As 377 compared with the models of TEMOM-log MOM (I) and (II), the TEMOM-log MOM 378 (I) has higher numerical accuracy. 379



380

# Fig. 4. Comparison of the geometric standard deviations of the particle number distributions derived from the family of TEMOM-log MOM.

The geometric standard deviation,  $\sigma_{g}$  of the particle number distribution (PSD) is a crucial indicator for characterizing the properties of PSD. The log MOM has the capability to directly produce the value of  $\sigma_{g}$  according to the first three moments (Lee et al., 1984). The other MOMs such as QMOM and TEMOM are verified to have the same capability of producing  $\sigma_{g}$  using the same moments as the log MOM

388 (Yu et al., 2008). Thus,  $\sigma_{g}$  can be used as an indicator to verify the investigated

methods. It is verified that this method has the ability to capture the polydispersity of particle size distribution. If an aerosol can be assumed to be a log-normal particle size distribution,  $\sigma_{g}$  can be expressed as a function of the first three moments (Pratsinis,

392 1988),

$$\ln^2 \sigma_{\rm g} = \frac{1}{9} \ln(\frac{M_0 M_2}{M_1^2}) \ (27)$$

In Fig. 4, the values of  $\sigma_g$  for various investigated methods are presented and 393 compared. The values of  $\sigma_g$  from all MOMs of the family of TEMOM-log MOM 394 achieve their own asymptotic values. The asymptotic value of  $\sigma_{\rm g}$  of TEMOM is 395 1.345, which is the closest to the value 1.346 produced by the QMOM with 6 nodes 396 (Yu et al., 2008). As expected, both the hybrid TEMOM-log MOM (I) and (II) models 397 achieve their asymptotic values. The values of  $\sigma_{\rm g}$  of the log MOM, and the hybrid 398 399 TEMOM-log MOM (I) and (II) models are 1.355, 1.365 and 1.315, respectively (Yu et al., 2008). The hybrid TEMOM-log MOM (I) model generates nearly the same 400  $\sigma_{\rm g}$  as the TEMOM and log MOM, whereas the hybrid TEMOM-log MOM (II) model 401 deviates from the other three investigated methods. It is concluded the hybrid 402 403 TEMOM-log MOM (I) model is a more precise method than the hybrid TEMOM-log MOM (II) by evaluating the four moments and their geometric standard deviations. 404 The TEMOM-log MOM (I) model has very nearly the same numerical precision as 405 the TEMOM and log MOM in numerical precision. 406

407 4.2 Numerical efficiency

# 408**Table 1** Computational time through executing the fourth-order Runge-Kutta409method with a fixed time step, 0.001.

Methods	Computational time
SM	~72.00 hour
TEMOM	~5.05 s
Log MOM	~6.00 s
TEMOM-log MOM (I)	~5.00 s
TEMOM-log MOM (II)	~8.08 s

The numerical precision and efficiency are equally important to determine the feasibility of any numerical models. Here, all the four investigated moment models as well as the SM, are implemented to  $\tau = 100$  The numerical efficiency of investigated models is also evaluated by comparing their computational times. For the SM, the section number is 500, which ensures the high numerical accuracy of this SM method.

Table 1 shows the computational time consumed by different investigated 415 models. The ODEs are all solved numerically by executing the fourth-order Runge-416 Kutta method with a fixed time step, 0.001 under an Intel(R) Core (TM) i7-3820 CPU 417 and Microsoft Visual Studio 2008. The time step, 0.001 is selected because the 418 419 numerical accuracy under the same time step has been validated in our previous study (Yu et al., 2008). Relative to all the MOMs, the SM consumes relatively very huge 420 computational time. The consumed time of the TEMOM-log MOM (I) model is 421 422 nearly the same as TEMOM but is smaller than log MOM and TEMOM-log MOM (II) models. By comparing Equations (22) with (22), the mathematical form of the 423 TEMOM-log MOM (II) is much more complex than that of the TEMOM-log MOM 424 (I), thus the former one needs more numerical calculations at each time step. 425 Therefore, it is concluded that the numerical efficiency of the TEMOM-log MOM (I) 426 model has clearly greater than the SM, log MOM and TEMOM-log MOM (II) 427 models, and is even greater than the well-known TEMOM. 428

In conclusion, the TEMOM-log MOM (I) model is verified to be a promising model for solving SCE in terms of both numerical efficiency and accuracy. In addition, this model has wider applications than the current log MOM because it overcomes the shortcoming of the log MOM with the pre-requirement of assumed log-normal particle size distribution. In the present study, the TEMOM-log MOM (I) model is utilized to study the secondary nanoparticle formation and subsequent growth in a turbulent jet plume in Section 4.3.

436 4.3 Application of the TEMOM-log MOM (I) model

In the atmospheric environment, it has been realized that most nanoparticles 437 come from a multicomponent route, i.e. binary homogeneous nucleation process of 438 439 water-sulfuric acid vapors, whereas a complete theoretical understanding of this phenomenon is still a challenge due to it's complicated chemical/physical processes 440 (Chan et al. 2010a and 2010b, Harrison et al., 2018; Liu & Chan, 2016; Maurya et al., 441 2018; Nagpure et al., 2011; Olin et al., 2019; Zhou & Chan, 2011). Due to the 442 unignorable contribution of gaseous and particulate emissions which are emitted from 443 the power plants and motor vehicles into the atmosphere (Chan, Liu, et al., 2010; 444 445 Chan, Zhou, et al., 2010; Chan & Ning, 2005; Ning et al., 2005a; Wang et al., 2006; Zhou & Chan, 2011), a lot of attention has been focused on the secondary particles. 446 Most of the particle number emitted by engines is in the nanoparticle range (i.e., 447  $d_p < 50$  nm), especially with the improvement of advanced engine technologies and 448

449 aftertreatment devices, much higher concentrations of nanoparticles than older

450 designs are produced nowadays. More and more evidence confirmed that these

- 451 nanoparticles might have a more negative effect on human health than micrometer
- and larger particles(Gnach et al., 2015; Harrison et al., 2018). This has raised a
- 453 question about how to control the emission of nanoparticles before and after the
- emission conditions. Hence, it is essential to have a better understanding the dynamic
- 455 processes of nanoparticle formation and subsequent growth in the atmospheric
- 456 environment.

The evolution of secondary particles in the exhaust is a complicated physicalchemical process, which involves the momentum, heat and mass transfer, binary homogeneous nucleation, Brownian coagulation, Brownian and turbulent diffusions, condensation and thermophoresis (Liu et al., 2019). The appropriate numerical model is coupled the Navier-Stokes equations for flows and the general dynamic equation for particles. The coupling is implemented in a one-way coupling way since nanoparticles have very little effect on the surrounding continuum.

464 4.3.1 Governing equations

#### 465 *4.3.1.1 Governing equations for fluid flow*

466 Nanoparticles have very small Stokes number in fluid flows to suggest that
467 particles can follow the fluid without disturbing it. In the present study, the Navier468 Stokes equations for incompressible flows are:

$$\frac{\partial u_i}{\partial x_i} = 0, \qquad (28(a))$$

$$\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left( v \frac{\partial u_i}{\partial x_j} \right), \qquad (28(b))$$

$$\frac{\partial \rho h}{\partial t} + \frac{\partial \rho h u_j}{\partial x_j} = \frac{\partial}{\partial x_j} \left( \frac{k_t}{C_p} \frac{\partial h}{\partial x_j} \right), \qquad (28(c))$$

where  $u_i$  is the velocity, p is the filtered pressure, h is the specific enthalpy,  $k_t$  is the thermal conductivity,  $C_p$  is the specific heat at constant pressure, the index i, j is taken as 1, 2 and refers to the x and y directions, respectively. The  $k - \varepsilon$  turbulent model scheme is utilized to solve Equation (28) regarding the effect of turbulence on the flow.

#### 474 *4.3.1.2 Governing equations for particles*

475 Within the Smoluchowski mean-field theory, the particle number concentration, 476 n(v,t), is represented as a function in terms of particle volume, v, and time, t. Taking 477 into consideration the physical terms of fluid convection, thermophoretic drift, 478 Brownian and turbulent diffusion, Brownian coagulation, condensation and

479 nucleation, the governing equation for n(v, t) can be expressed as:

$$\frac{\partial n(v,t)}{\partial t} + \frac{\partial \left(u_{j}n(v,t)\right)}{\underbrace{\partial x_{j}}_{\text{convection}}} + \frac{\partial \left((u_{th})_{j}n(v,t)\right)}{\underbrace{\partial x_{j}}_{\text{thermophoresis}}} = \frac{\partial}{\frac{\partial x_{j}}{\left(\Gamma \frac{\partial n(v,t)}{\partial x_{j}}\right)}}{\frac{\partial x_{j}}{\frac{\partial x_{j}}{\frac{x_{j}}{\frac{\partial x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac{x_{j}}{\frac$$

where *G* is the growth rate of nucleus volume due to condensation,  $\Gamma$  is the sum of the turbulent diffusion and Brownian diffusion coefficients ( $\Gamma = \Gamma_t + \Gamma_B$ ),  $\beta(v, v')$  is the coagulation kernel between particles of two volumes as shown in Equation (2), *J* is the nucleation rate,  $v^*$  is the volume of a stable sulfuric acid-water (H<sub>2</sub>SO<sub>4</sub>-H<sub>2</sub>O) monomer,  $\delta$  is the Kronecker Delta function and  $u_{th}$  is the thermophoretic velocity.

The Equation (29) is usually called the general dynamics equation (GDE), which cannot be directly coupled with Equation (28) for calculation due to its too many degrees relative to the particle volume v. In order to overcome the shortcoming of the GDE, the suitable numerical scheme is to transfer Equation (29) with respect to  $\{n(v, t)\}$  to the moment  $\{m_k\}$ . The moment transformation involves multiplying Equation (29) by v and then integrating over the entire particle size distribution, and then the governing equation for the k —th moment is expressed as,

$$\frac{\partial m_k}{\partial t} + \frac{\partial (u_j + (u_{th})_j)m_k}{\partial x_j}$$
$$= \frac{\partial}{\partial x_j} \left( \Gamma \frac{\partial m_k}{\partial x_j} \right) + k B_1 \hbar m_{k-\frac{1}{3}} \frac{1}{\alpha} + J(v^*) v^{*k}$$
$$+ \left[ \frac{\partial m_k}{\partial t} \right]_{\text{coag}} (k = 0, 1, 2) \quad (30)$$

493

494 where  $\left[\frac{\partial m_k}{\partial t}\right]_{\text{coag}}$  is calculated using the Equation (20) of TEMOM-log MOM (I)

495 model. For the unresolved moment,  $m_{k-1/3}$  in Equation (30), the closure model in

496 Equation (19) needs to be used to achieve the final closure of equations. In the

497 implementation of TEMOM-log MOM (I) model, only the first three order moments498 need to be explicitly solved.

499 Many studies have indicated that sulfuric acid tends to gather water molecules 500 around to form hydrates. These hydrates are considered to stabilize the vapor and 501 reduce the nucleation rate by a factor  $10^3 \sim 10^8$  (Vehkamaki et al., 2003). In the present study, the advanced parameterization model of Vehkamaki et al. (2003) accounting for high-temperature emissions is used, which is verified to be suitable for the study of particulate matters emitted from engine (Yu et al., 2009). In this new model, the key variables such as nucleation rate  $J(v^*)$ , the mole fraction and the total number of molecules of sulfuric acid in a critical cluster are taken as functions of temperature, relative humidity and total gas-phase concentration of sulfuric acid.

508 In the model of Vehkamaki et al. (2003), the mole fraction of sulfuric acid 509  $x^*$  in a critical cluster is given by

510

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\begin{aligned} x^* &= 0.847012 - 0.0029656T - 0.00662266\ln(Na) + 0.0000587835T\ln(Na) \\ &+ 0.0592653\ln(RH) - 0.000363192T\ln(RH) + 0.0230074(\ln(RH))^2 \\ &+ 0.0000851374T(\ln(RH))^2 + 0.00217417(\ln(RH))^2 \\ &- 7.923 \times 10^{-6}T(\ln(RH))^3 \end{aligned}
```

511

512 where Na is the total gas-phase concentration of sulfuric acid, T is the absolute

temperature and RH is the relative humidity in percentage. The nucleation rate is

- given by an exponential of a third-order polynomial of  $\ln(RH)$  and  $\ln(Na)$
- 515

 $J(v^*) = \exp[a(T, x^*) + b(T, x^*)\ln(RH) + c(T, x^*)(\ln(RH))^2 + d(T, x^*)(\ln(RH))^3$  $+ e(T, x^*)\ln(Na) + f(T, x^*)\ln(RH)\ln(Na) + g(T, x^*)(\ln(RH))^2\ln(Na)$  $+ h(T, x^*)(\ln(Na))^2 + i(T, x^*)\ln(RH)(\ln(Na))^2 + j(T, x^*)(\ln(Na))^3$ (32)

(31)

516

517 where the coefficients  $a(T, x^*) \dots j(T, x^*)$  are functions of temperature *T* and critical 518 cluster mole fraction  $x^*$ . The total number of molecules in the critical cluster N<sup>\*</sup><sub>tot</sub> is 519 given by

520

 $N_{\text{tot}}^* = \exp[A(T, x^*) + B(T, x^*)\ln(RH) + C(T, x^*)(\ln(RH))^2 + D(T, x^*)(\ln(RH))^3$  $+ E(T, x^*)\ln(Na) + F(T, x^*)\ln(RH)\ln(Na) + G(T, x^*)(\ln(RH))^2\ln(Na)$  $+ H(T, x^*)(\ln(Na))^2 + I(T, x^*)\ln(RH)(\ln(Na))^2 + J(T, x^*)(\ln(Na))^3$ (33)

521

where the coefficients  $A(T, x^*) \dots J(T, x^*)$  are also functions of temperature *T* and critical cluster mole fraction  $x^*$ . The detailed definitions for these coefficients can be found in the study of Vehkamaki et al. (2003).

525 In addition, several key functions or parameters, including the velocity of 526 thermophoresis,  $u_{th}$ , subgrid-scale turbulent diffusivity coefficient,  $\Gamma_t$ , and Brownian 527 diffusion coefficient,  $\Gamma_b$ , the growth rate of particle size due to the arrival and loss of 528 the sulfuric acid (H<sub>2</sub>SO<sub>4</sub>) molecules to the entire droplet surface, *G*, can be found in 529 (Liu et al., 2019).

530 *4.3.1.3 Governing equations for gas species* 

531 During the numerical simulation, the evolution of gas species including 532 sulfuric acid and water vapors, must be determined before making the calculation of 533 moment ODEs. Based on the moment transformation in Equation (4), the differential equations for the evolution of gas species, including sulfuric acid,  $Y_1$ , water vapors,  $Y_2$ , and CO<sub>2</sub> tracer,  $Y_3$  are expressed as:

$$\frac{\partial Y_1}{\partial t} + \frac{\partial u_j Y_1}{\partial x_j} = \frac{\partial}{\partial x_j} \left( D_1 \frac{\partial Y_1}{\partial x_j} \right) + R - J(v^*)k^* - \frac{B_1}{v^*}\hbar m_{2/3}$$
(34(a))

$$\frac{\partial Y_2}{\partial t} + \frac{\partial u_j Y_2}{\partial x_j} = \frac{\partial}{\partial x_j} \left( D_2 \frac{\partial Y_2}{\partial x_j} \right)$$
(34(b))

$$\frac{\partial Y_3}{\partial t} + \frac{\partial u_j Y_3}{\partial x_j} = \frac{\partial}{\partial x_j} \left( D_3 \frac{\partial Y_3}{\partial x_j} \right)$$
(34(c))

- where  $k^*$  is the number of sulfuric acid molecules in the critical cluster which is
- 537 denoted by  $k^* = N_{tot}^* \cdot x^*$ , and *R* is the birth rate.  $D_1$ ,  $D_2$  and  $D_3$  are molecular
- diffusion coefficients of sulfuric acid, water vapors and  $CO_2$  tracer respectively.  $k^*$  is
- obtained from the nucleation model of Vehkamaki et al. (2003).

540

4.3.1.4 Configuration of the computational domain



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## Figure 5 Cartesian coordinate system (*x*, *y*, *z*) of the computational domain

544 Fig.5 is the Cartesian coordinate system (x, y, z) used in the numerical simulations for the vehicle exhaust plume, which is consistent with the experimental 545 setup shown in (Ning et al., 2005b) and the same as the numerical calculation shown 546 in Yu et al. (2009). The diameter of the vehicle tailpipe is D = 0.03 m. The 547 computational domain is 1000D in x-coordinate  $\times$  333D in y-coordinate. In order to 548 make comparison with the experimental data and the previous numerical calculation 549 data using the TEMOM model, the tailpipe exit velocity used is 4.8 m/s and the 550 exhaust temperature used is 400 K; H<sub>2</sub>O and CO<sub>2</sub> are accounted for 6% and 12% in 551 mole fraction, respectively. The velocity of surrounding air is taken as 0 m/s for the 552 present numerical simulation. The numerical calculation is simplified to be a two-553 dimensional axisymmetric model which the vehicle tailpipe is a circular pipe. 554

555	All the governing equations are discretized by the finite-volume method. The
556	Quadratic Upwind Interpolation for Convective Kinematics (QUICK) scheme is
557	adopted for the convective terms in Equations (28), (30) and (34). For the governing
558	equations accounting for particles and gas species in Equations (30) and (34), a user-
559	defined functions (UDF) in ANSYS Fluent are utilized. The TEMOM-log MOM (I)
560	in Equation (20) is utilized to calculate the evolution of nanoparticle dynamics due to
561	Brownian coagulation. The calculation time step t is fixed to be 0.001 s for all the
562	numerical simulations regarding both the numerical efficiency and accuracy. In the
563	numerical simulation, all calculations are implemented using normalized parameters:
564	the details for the normalization are the same as in our previous research works (Liu
565	et al. Liu. 2019: Yu et al. 2009)
505	et al. Ela, 2019; 1a et al., 2009).
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Figure 6 The contours of (a) the velocity magnitude (m/s)), (b) the normalized secondary particle number concentration,  $M_0$ , (c) normalized particle volume concentration,  $M_1$  and (d) nucleation rate of secondary particles,  $J(v^*)$  (#/(s·m<sup>3</sup>).



(c) Figure 7 The radial distance, y (m) of (a) the normalized secondary particle number concentration,  $M_0$ , (b) normalized particle volume concentration,  $M_1$  and (c) nucleation rate of secondary particles at the axial tailpipe exit, x/D = 3.33, 16.67, 33.33 and 66.66. Red dot line = 3.33, Pink dot line = 16.67, Green dot line = 33.33 and blue dot line = 66.66 in Figures 6(a), (b) &(c).

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- 595

Figure 6 shows the distribution of (a) the velocity magnitude, (b) normalized secondary 596 particle number concentration, (c) normalized particle volume concentration and (d) nucleation 597 rate of secondary particles. It should be noted both  $M_0$  and  $M_1$  shown in Figures 6(b) and (c) are 598 599 normalized values according to the normalized equation presented in Eq. (23). In the turbulent jet flow, the evolution of large vortex is found to dominate the distribution and evolution of particle 600 quantities, including the particle number concentration, particle volume concentration, averaged 601 particle size and geometric standard deviation of particle number distribution in the surrounding 602 air condition (Garrick & Khakpour, 2004; Lin et al., 2016). 603

The effect of the large vortex on the distribution of statistical moment quantities are 604 represented in Figures 6(b) and (c), where the maximum value of particle number concentration 605 appears at the near tailpipe exit  $x \approx 0.25 \sim 0.35$  m due to the strong mixture between the exhaust 606 jet flow and the surrounding cold air occurs. In the jet region, the exhaust jet plume temperature 607 decreases to a lower level due to the mixing with the surrounding cold air, and makes the 608 occurrence of binary homogeneous nucleation. It also leads to the high nucleation rate for 609 H<sub>2</sub>SO<sub>4</sub>-H<sub>2</sub>O monomers occurs there, so as the high concentration for the particle number 610 611 concentration as shown in Figure 6(b). However, it is not surprisingly observed that the main nucleation rate appears only at near tailpipe exit region as shown in Figure 6(d) especially the 612 region is much closer to the tailpipe exit than the high particle number concentration region as 613 614 shown in Figure 6(b). Further exhaust jet flow downstream, eddies form and entrain the surrounding cold air into the main exhaust jet flow and decrease the gas temperature in the 615 mixing region but no high particle number concentration is formed. 616

In Figure 6(c), it can be observed that the particle mass concentration reaches the maximum 617 value away from the tailpipe exit at  $x \approx 0.50 \sim 0.70$  m. Contrary to the particle number 618 distribution and nucleation rate, the particle mass distribution mainly distributes in the centerline 619 of exhaust jet flow rather in the jet interface. The evolution and distribution of particle dynamics 620 obtained in this study is consistent with the results obtained from the transient method, such as 621 large eddy simulation (Yu et al., 2009), which is the result of external effect such as convection, 622 diffusion and thermophoresis, and the internal dynamic processes (i.e., nucleation, condensation 623 and coagulation). In research group of Garrick (Garrick, 2011; Miller & Garrick, 2004; Murfield 624 & Garrick, 2013) on nanoparticle-laden jet and boundary flows, the new formation of particles 625 on the turbulent interface in boundary layers is also observed, which is considered to be the main 626 source of particle formation in a turbulent flow. 627

The radial distance of normalized  $M_0$  and  $M_1$ , and nucleation rate at different axial exhaust 628 jet distances from the tailpipe exit are shown in Figure 7. Both the newly proposed TEMOM-log 629 MOM (I) model and the widely recognized log MOM model are implemented for the 630 comparative study. There are no obvious difference in the investigated three physical quantities 631 for both MOMs. It should be noted the log MOM is still now the most widely used method in 632 the atmospheric aerosol dynamics due to its high numerical efficiency, for example WRF-Chem 633 in the field of earth science. In Figures 7(a) and (b), it is clear in the region very close to the 634 tailpipe exit, i.e. x = 0.1 m, the values of both  $M_0$  and  $M_1$  reach their maximum at the region 635 away from the centerline of the exhaust jet flow, while further exhaust jet flow downstream, 636 x = 0.5 to 2.0 m, the values of both  $M_0$  and  $M_1$  in the centerline region of exhaust jet flow are 637

larger than that in the surrounding region. It implies that in the downstream region, the

- surrounding air is entrained by large vortices into the nanoparticle-laden multiphase system,
- which dominates the evolution of the particle dynamics rather than the nucleation process. In
- Figure 7(c), the nucleation process only appears at x = 0.1 and 0.2 m, while further exhaust jet flow downstream at x = 1.0 m and 2.0 m, no new particle formation takes place. This is further
- verified the conclusion from Figure 6(d) that in only the region which new particle can be
- formed at very near region to the tailpipe exit. In addition, it is clear that the nearer to the
- tailpipe exit, the higher nucleation rate is formed. The finding would be contrary to the common
- knowledge that new particles are mostly formed in the region where the jet and the surroundingcold air can be strongly mixed in the downstream exhaust jet flow region (Lin et al., 2016). In
- the present study, only new particle formation is observed in the jet flow boundary which is very
- close to the tailpipe exit, while in the downstream exhaust jet flow region where the strong
- mixture is achieved but no new particle formation is observed. This should contribute to the fact that the number concentration formed of new particles by the main precursor (i.e.,  $H_2SO_4$  vapor)
- that the number concentration formed of new particles by the main precursor (i.e.,  $H_2SO_4$  vapor) cannot meet the minimum requirement to achieve thermally stable  $H_2SO_4$ -  $H_2O$  monomer in the
- 653 exhaust jet flow downstream.

#### 654 **5 Conclusions**

In the present study, a new mathematical method for solving the SCE undergoing Brownian 655 656 coagulation in the free molecular regime is firstly proposed and developed. In this method, the concept of well-established TEMOM and log MOM for approximating collision kernel and 657 implicit moments are hybridized. The numerical precision and efficiency of the new method are 658 evaluated by comparing to the SM as well as the TEMOM and classic log MOM. The results 659 imply that the new method in which the collision kernel is approximated with the concept of log 660 MOM and the implicit moments are closed by the concept of TEMOM which has nearly the 661 same numerical precision and efficiency as the TEMOM and log MOM. This new method is 662 further successfully applied to the study of secondary nanoparticle formation and subsequent 663 growth of H<sub>2</sub>SO<sub>4</sub>-H<sub>2</sub>O in a turbulent jet plume. With the new method, the formation of new 664 particles only appears in the interface region of the turbulent exhaust jet which is very close to 665 the tailpipe exit, while there is no new particle formation in the strong mixture between the 666 exhaust jet plume and the surrounding cold air along the downstream. The new method 667 overcomes the limitation of the classical log MOM that the particle size distribution must follow 668 log-normal particle size distributions with respect to time. Thus this new method provides wide 669 applications where the atmospheric aerosol size distribution is typical bimodal or multi-modal 670 cases. 671

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TEMOM-log MOM method have been archived in the Mendeley data with a name "A hybrid

677 TEMOM-log MOM Method".

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### 679 **7** Appendix

680 7.1 The derivation of Equation (11)

$$\begin{split} \beta(v,v_1) &= K(1/v+1/v_1)^{\frac{1}{2}} (v^{\frac{1}{3}}+v_1^{\frac{1}{3}})^2 \\ &= K(v+v_1)^{\frac{1}{2}} (v^{\frac{1}{6}}v_1^{-\frac{1}{2}}+2v^{-\frac{1}{6}}v_1^{-\frac{1}{6}}+v^{-\frac{1}{2}}v_1^{\frac{1}{6}}) \\ &\approx Kb_k (v^{\frac{1}{2}}+v_1^{\frac{1}{2}}) (v^{\frac{1}{6}}v_1^{-\frac{1}{2}}+2v^{-\frac{1}{6}}v_1^{-\frac{1}{6}}+v^{-\frac{1}{2}}v_1^{\frac{1}{6}}) \\ &= Kb_k (v^{\frac{2}{3}}v_1^{-\frac{1}{2}}+2v^{\frac{1}{3}}v_1^{-\frac{1}{6}}+v_1^{\frac{1}{6}}+v^{\frac{1}{6}}+2v^{-\frac{1}{6}}v_1^{\frac{1}{3}}+v^{-\frac{1}{2}}v_1^{\frac{2}{3}}) \\ &\triangleq \tilde{\beta}_{\text{Log}}(v,v_1) \end{split}$$
(A1)

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682 7.2 The derivation of Equation (16)

$$\begin{split} \beta(v,v_{1}) \\ &= K(1/v+1/v_{1})^{\frac{1}{2}}(v^{\frac{1}{3}}+v_{1}^{\frac{1}{3}})^{2} \\ &= K(v+v_{1})^{1/2}(v^{1/6}v_{1}^{-1/2}+2v^{-1/6}v_{1}^{-1/6}+v^{-1/2}v_{1}^{1/6}) \\ &\approx K(\frac{3\sqrt{2u}}{8}+\frac{3\sqrt{2v}}{8\sqrt{u}}+\frac{3\sqrt{2}v_{1}}{8\sqrt{u}}-\frac{\sqrt{2}v^{2}}{32u^{\frac{3}{2}}}-\frac{\sqrt{2}vv_{1}}{16u^{\frac{3}{2}}}-\frac{\sqrt{2}v^{2}}{32u^{\frac{3}{2}}})(v^{\frac{1}{6}}v_{1}^{-\frac{1}{2}}+2v^{-\frac{1}{6}}v_{1}^{-\frac{1}{6}}+v^{-\frac{1}{2}}v_{1}^{\frac{1}{6}}) \\ &= K\left[\frac{3}{8}(2u)^{\frac{1}{2}}(2v^{\frac{1}{6}}v_{1}^{-\frac{1}{2}}+2v^{-\frac{1}{6}}v_{1}^{-\frac{1}{6}})+\frac{3}{8}(\frac{2}{u})^{\frac{1}{2}}(2v^{\frac{7}{6}}v_{1}^{-\frac{1}{2}}+4v^{\frac{5}{6}}v_{1}^{-\frac{1}{6}}+2v^{\frac{1}{2}}v_{1}^{\frac{1}{6}}) \\ &-\frac{1}{32}(\frac{2}{u^{3}})^{\frac{1}{2}}(4v^{\frac{5}{6}}v_{1}^{\frac{5}{6}}+4v^{\frac{7}{6}}v_{1}^{\frac{1}{2}}+2v^{\frac{3}{2}}v_{1}^{\frac{1}{6}}+2v^{\frac{13}{6}}v_{1}^{-\frac{1}{2}}+4v^{\frac{11}{6}}v_{1}^{-\frac{1}{6}})\right] \\ &\triangleq \tilde{\beta}_{\text{Taylor}}(v,v_{1}) \end{split} \tag{A2}$$

684 7.3 The derivation of Equation (23)

 $^{685}$  The *k*-th moment with closure function by assuming the log-normal particle size distribution  $^{686}$  takes the following expression

$$m_k = \int_0^\infty e^{ky} \cdot \frac{N_0}{3\sqrt{2\pi}\ln\sigma} e^{-\frac{(y-\ln v_g)^2}{18\ln^2\sigma}} dy$$
$$= \frac{N_0}{3\sqrt{2\pi}\ln\sigma} \int_0^\infty e^{-\frac{y^2 - 2(\ln v_g + 9k\ln^2\sigma)y + \ln^2 v_g}{18\ln^2\sigma}} dy$$

$$= e^{k \ln v_g + \frac{9}{2}k^2 \ln^2 \sigma} \cdot \frac{N_0}{3\sqrt{2\pi} \ln \sigma} \int_0^\infty e^{-\frac{(y - \ln v_g - 9k \ln^2 \sigma)^2}{18 \ln^2 \sigma}} dy$$
  
=  $m_0 e^{k \ln(v_g) + \frac{9}{2}k^2 \ln^2 \sigma}$  (A3)

where  $N_0(=m_0)$  is the initial total number of particles,  $v_g$  is the geometric mean volume.

Equation (A3) can be further expressed in terms of  $m_0$ ,  $m_1$  and  $m_2$ :

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$$m_k = m_0^{1 - \frac{3}{2}k + \frac{1}{2}k^2} m_1^{2k - k^2} m_2^{-\frac{1}{2}k + \frac{1}{2}k^2}.$$

691 7.4 Normalized moment ODEs

When the Equation (25) is introduced into Equations (20) and (22), the normalized equations for the hybrid models (I) and (II) are obtained as, respectively,

$$\begin{cases} \frac{\mathrm{d}M_0}{\mathrm{d}\tau} = -\frac{\sqrt{2}M_0^{\frac{59}{36}}}{32M_1^{\frac{29}{9}}M_2^{\frac{7}{36}}} \begin{pmatrix} -\frac{11}{6}M_1^{\frac{1}{9}}M_2^{\frac{11}{6}} + 12M_0^{\frac{2}{3}}M_1^{\frac{29}{9}}M_2^{\frac{2}{3}} + 11M_0^{\frac{1}{2}}M_2^{\frac{19}{9}}M_2^{\frac{1}{2}} + 12M_0^{\frac{7}{18}}M_1^{\frac{3}{1}}M_2^{\frac{7}{2}} \\ + 24M_0^{\frac{9}{9}}M_1^{\frac{3}{3}}M_2^{\frac{9}{2}} - 2M_0^{\frac{11}{6}}M_1^{\frac{19}{9}}M_2^{\frac{1}{6}} - 2M_0^{\frac{19}{18}}M_1^{\frac{19}{3}}M_2^{\frac{19}{18}} - 2M_0^{\frac{11}{18}}M_1^{\frac{11}{3}}M_2^{\frac{11}{18}} + 12M_1^{\frac{9}{9}} \end{pmatrix} \\ -\frac{\mathrm{d}M_1}{\mathrm{d}\tau} = 0 \\ \frac{\mathrm{d}M_2}{\mathrm{d}\tau} = -\frac{\sqrt{2}M_0^{-\frac{25}{36}}}{16M_1^{\frac{41}{9}}M_2^{\frac{5}{36}}} \begin{pmatrix} M_0^{\frac{23}{6}}M_1^{\frac{19}{9}}M_2^{\frac{31}{9}} - 24M_0^{\frac{11}{9}}M_1^{\frac{16}{3}}M_2^{\frac{5}{6}} - 12M_0^{\frac{5}{3}}M_1^{\frac{49}{9}}M_2^{\frac{23}{18}} + 2M_0^{\frac{13}{6}}M_1^{\frac{39}{9}}M_2^{\frac{19}{9}} + 2M_0^{\frac{5}{18}}M_1^{\frac{3}{3}}M_2^{\frac{8}{9}} \end{pmatrix} \\ -\frac{\mathrm{d}M_1}{\mathrm{d}\tau} = 0 \\ \frac{\mathrm{d}M_2}{\mathrm{d}\tau} = -\frac{\sqrt{2}M_0^{-\frac{25}{36}}}{16M_1^{\frac{41}{9}}M_2^{\frac{5}{36}}} \begin{pmatrix} M_0^{\frac{23}{6}}M_1^{\frac{9}{9}}M_2^{\frac{39}{9}} - 24M_0^{\frac{11}{9}}M_1^{\frac{16}{3}}M_2^{\frac{5}{6}} - 12M_0^{\frac{5}{3}}M_1^{\frac{49}{9}}M_2^{\frac{23}{18}} + 2M_0^{\frac{13}{6}}M_1^{\frac{19}{9}}M_2^{\frac{9}{9}} + 2M_0^{\frac{5}{18}}M_1^{\frac{3}{3}}M_2^{\frac{8}{9}} \end{pmatrix} \\ +2M_0^{\frac{37}{18}}M_1^{\frac{11}{3}}M_2^{\frac{5}{2}} + M_0^{\frac{25}{9}}M_1^{\frac{9}{9}}M_2^{\frac{9}{9}} - 12M_0^{\frac{16}{9}}M_1^{\frac{9}{9}}M_2^{\frac{9}{9}} - 12M_0M_1^{\frac{19}{9}}M_2^{\frac{11}{9}} - 12M_0M_1^{\frac{5}{9}}M_2^{\frac{11}{9}} - 12M_0M_0M_1^{\frac{5}{9}}M_2^{\frac{11}{9}} - 12M_0M_0M_1^{\frac{5}{9}}M_2$$

(A4)

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695 and

$$\begin{cases} \frac{dM_0}{d\tau} = b \frac{M_0^{11/6} (41M_0^2 M_2^2 - 190M_0 M_1^2 M_2 - 2443M_1^4)}{648M_1^{23/6}} \\ \frac{dM_1}{d\tau} = 0 \\ \frac{dM_2}{d\tau} = -b \frac{65M_0^2 M_2^2 - 670M_0 M_1^2 M_2 - 1987M_1^4}{324M_0^{1/6} M_2^{11/6}}. \end{cases}$$
(A5)

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